

# Transformation of Data

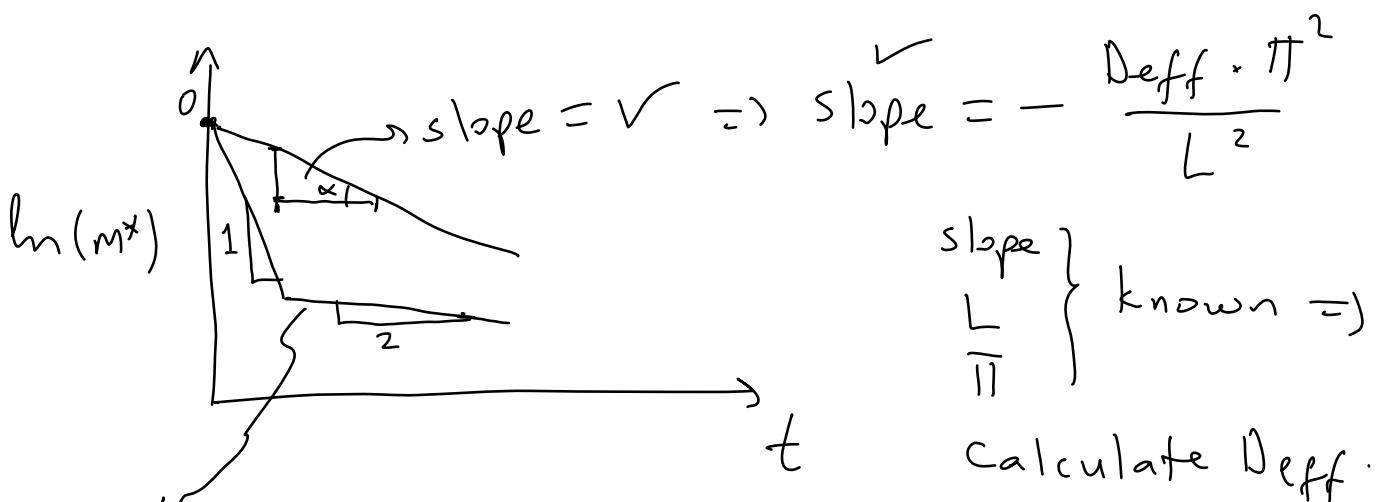
\*  $D_{eff}$  is typically determined by plotting experimental drying data vs time.

$$\begin{array}{ccc} \frac{X}{\vdots} & \frac{t}{\vdots} & \frac{m^*}{\vdots} \\ & \Rightarrow \text{calculate} & \end{array}$$

For a sphere  $\Rightarrow$

$$m^* = \frac{X - X^*}{X_0 - X^*} = \frac{6}{\pi^2} \cdot \exp\left(-\frac{D_{eff} \cdot \pi^2 \cdot t}{L^2}\right)$$

$$\ln(m^*) = \ln\left(\frac{6}{\pi^2}\right) - \frac{D_{eff} \cdot \pi^2 \cdot t}{L^2} \quad \leadsto \text{linear eqn}$$



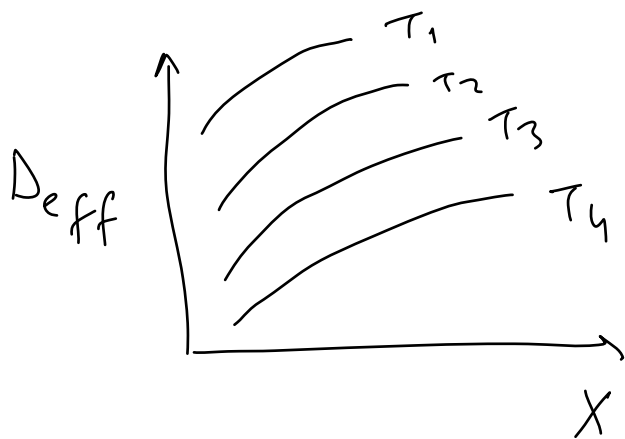
two falling rates  $\Rightarrow D_{eff1}$  and  $D_{eff2}$   $\quad \_$

$$D_{eff1} > D_{eff2}$$

\*  $D_{eff}$  changes with MC and T.

as  $T \nearrow \Rightarrow D_{eff} \nearrow$

as  $MC \downarrow \Rightarrow D_{eff} \downarrow$



$$T_1 > T_2 > T_3 > T_4$$

\* The temperature dependence of diffusivity is described by an Arrhenius type equation.

$$D_{eff} = D_0 \times \exp\left(-\frac{E_a}{RT}\right)$$

$D_0$ : diffusivity constant.

when  $T \rightarrow \infty \Rightarrow D_{eff} \approx D_0$

$E_a$ : activation energy (kJ/mol)

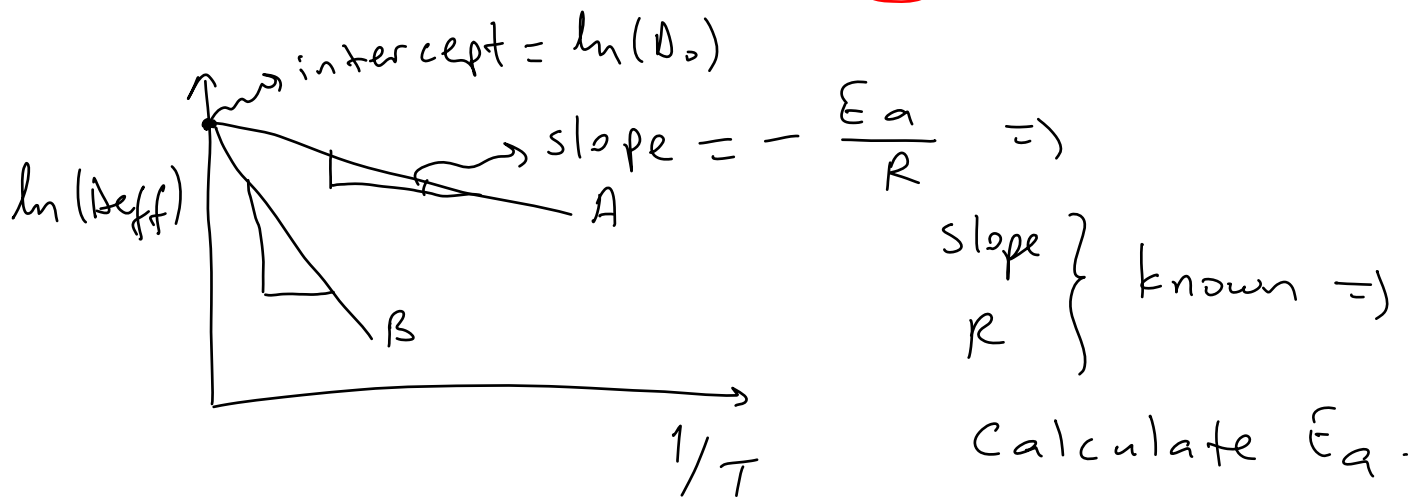
$R$ : gas constant (8.314 kJ/mol.K)

$T$ : absolute temp. (K).

⊗  $E_a$  values are in the range of  $15 - 40 \frac{\text{kJ}}{\text{mol}}$  for various foods.

⊗ The  $E_a$  can be determined by plotting  $\ln(D_{\text{eff}})$  vs  $1/T$ .

$$\ln(D_{\text{eff}}) = \ln(D_0) - \frac{E_a}{R} \cdot \frac{1}{T}$$



The food B is more  $T$  sensitive than A.

i.e.,  $D_{\text{eff}}$  values of B varies with  $T$  easily than A.

i.e., it is not necessary to dry A at very high  $T$ 's. Because  $D_{\text{eff}}$  value doesn't change with  $T$ . It is important to dry it at possible minimum temperatures in order to save energy and keep the quality properties of food at high levels.

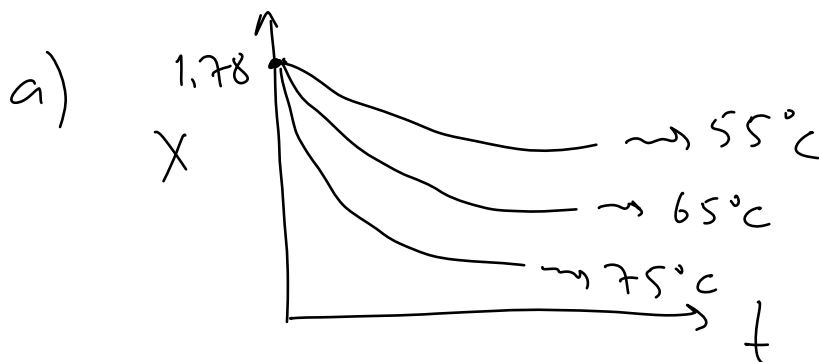
**Example: 2.78 kg of grape leather (initial MC = 64 % wb) with a thickness of 1 mm was spread on a  $0.06 \text{ m}^2$  area and dried in a tray dryer using hot air. A typical time (min)-MC (kg  $\text{H}_2\text{O}$ /kg dry solids) data was obtained as shown below:**

- Plot MC vs time
- Plot drying rate ( $\text{kg H}_2\text{O}/\text{m}^2 \cdot \text{min}$ ) vs MC
- Estimate diffusivity values
- Estimate  $E_a$  value.

Data:

<u>t (min)</u>	<u><math>X</math> (75°C) <sup>db</sup></u>	<u><math>X</math> (65°C)</u>	<u><math>X</math> (55°C)</u>
0	1.78	1.78	1.78
10	0.85	1.19	1.31
20	0.36	0.71	1.00
30	0.21	0.39	0.61
40	0.13	0.22	0.39
50	0.11	0.14	0.23
60	0.098	0.11	0.18

Solution:

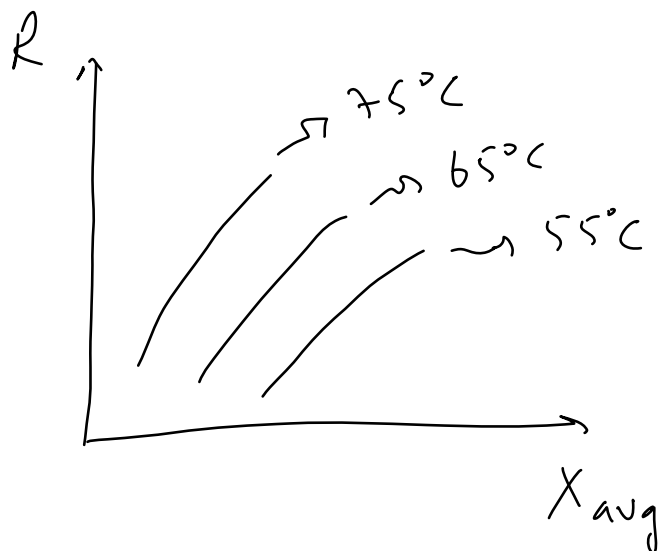


$$b) R = - \frac{M_s}{A} \times \frac{(X_{i+1} - X_i)}{(t_{i+1} - t_i)}$$

$$M_s = 2.78 \times (1 - 0.64) \cong 1.0 \text{ g DS.}$$

$$\frac{M_s}{A} = \frac{1}{0.06} = 166.6 \text{ kg DS/m}^2 = \text{constant.}$$

$(t_{i+1} - t_i)$	$(X_{i+1} - X_i)$			$X_{\text{average}}$			$R$		
	<u>75°C</u>	<u>65°C</u>	<u>55°C</u>	<u>75</u>	<u>65</u>	<u>55</u>	<u>75</u>	<u>65</u>	<u>55</u>
10 →	-0.93	⋮	⋮	→ 1.315	⋮	⋮	→ 15.5	⋮	⋮
10 →	-0.49	⋮	⋮	→ 0.605	⋮	⋮	→ 8.16	⋮	⋮
10 →	-0.15		→	0.285		→	2.5		
10 →	-0.08		→	0.17		→	1.33		
10 →	-0.02		→	0.12		→	0.33		
10 →	-0.012		→	0.104		→	0.2		



} drying is in the falling rate period.

Calculate  $t_f \Rightarrow$

$$t_f = \frac{M_s}{A} \left( \frac{x_1 - x_2}{R_1 - R_2} \right) \times \ln \frac{R_1}{R_2}$$

$$t_{75} = 166.6 \frac{\text{kg DS}}{\text{m}^2} \times \frac{(1.315 - 0.104) \frac{\text{kg H}_2\text{O}}{\text{kg DS}}}{(15.5 - 0.2) \frac{\text{kg H}_2\text{O}}{\text{m}^2 \cdot \text{min}}} \times \ln \left( \frac{15.5}{0.2} \right)$$

$$t_{75^\circ\text{C}} \approx 57.4 \text{ min.}$$

$t_{65}$  and  $t_{55} \Rightarrow$  calculate at home.

c) Assume slab shape  $\Rightarrow$

$$m^* = \frac{x - x^*}{x_0 - x^*} = \frac{8}{\pi^2} \exp \left( - \frac{\pi^2 \cdot \text{Deff} \cdot t}{4 \times L^2} \right)$$

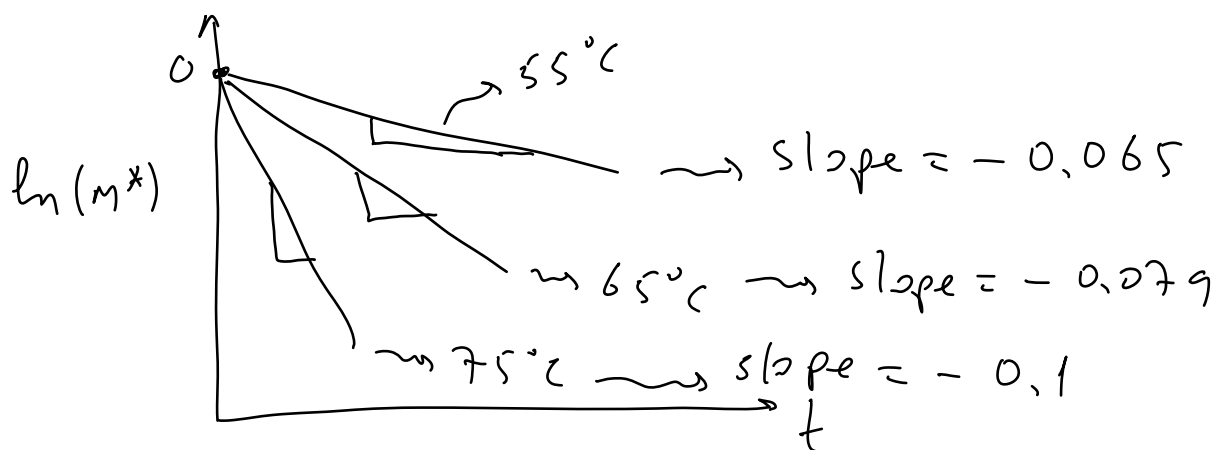
$$\ln(m^*) = \ln \left( \frac{8}{\pi^2} \right) - \frac{\pi^2 \cdot \text{Deff} \cdot t}{4 \times L^2}$$

$T$	$x_0$	$x^*$
75 $\rightarrow$	1.78	0.098
65 $\rightarrow$	"	0.11
55 $\rightarrow$	"	0.18

for  $75^\circ\text{C} \Rightarrow$

$t$	$m^*$
0 $\rightarrow$	1
10 $\rightarrow$	0.44
20 $\rightarrow$	0.15
$\vdots$	$\vdots$
60	.

<u>t</u>	<u>m*</u>			<u>ln(m*)</u>		
	<u>75°C</u>	<u>65°C</u>	<u>55°C</u>	<u>75</u>	<u>65</u>	<u>55</u>
0 →	1	1	1	0	0	0
10 →	0.44	⋮	⋮	→ -0.80	⋮	⋮
20 →	0.15			→ -1.85		
30 →	0.06			→ -2.7		
40 →	0.01			→ -3.9		
50 →	0.007			→ -4.9		
60 →	0			→ ∞		



$$\text{slope} = - \frac{D_{\text{eff}} \cdot \pi^2}{4 \times L^2}$$

$$\text{For } 55^\circ\text{C} \Rightarrow -0.065 = - \frac{D_{\text{eff}} \cdot \pi^2}{L \times (1 \times 10^{-3})^2 \text{ m}^2} \Rightarrow$$

$$D_{\text{eff}} \text{ at } 55^\circ\text{C} = 2.63 \times 10^{-8} \text{ m}^2/\text{min}$$

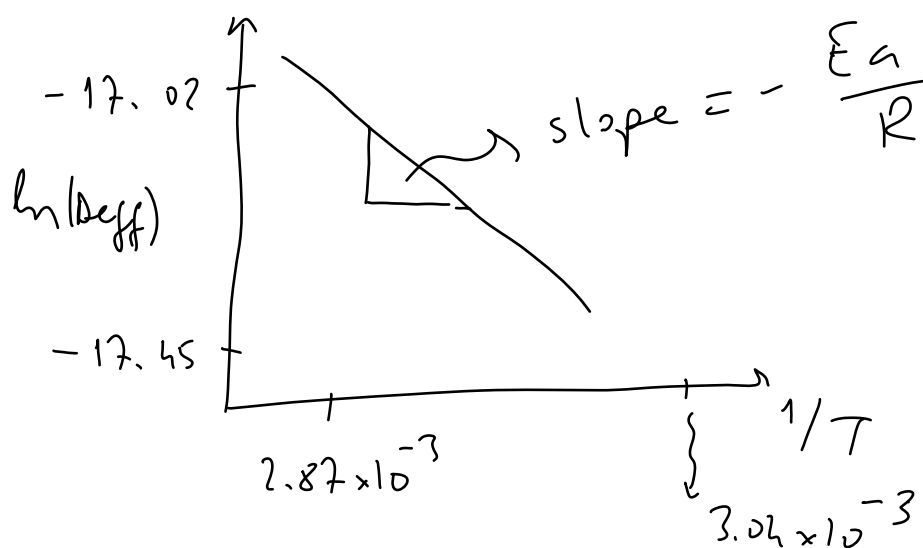
$$D_{\text{eff}} \text{ at } 65^\circ\text{C} = 3.2 \times 10^{-8} \text{ m}^2/\text{min}$$

$$D_{\text{eff}} \text{ at } 75^\circ\text{C} = 4.056 \times 10^{-8} \text{ m}^2/\text{min}$$

$$d) D_{eff} = D_0 \times \exp\left(-\frac{E_a}{RT}\right) \Rightarrow$$

$$\ln(D_{eff}) = \ln(D_0) - \frac{E_a}{RT}$$

$T$	$1/T$	$D_{eff}$	$\ln(D_{eff})$
$75 + 273$	$\rightarrow 2.87 \times 10^{-3}$	$\rightarrow 4.056 \times 10^{-8}$	$\rightarrow -17.02$
$65$	$\rightarrow 2.95 \times 10^{-3}$	$\rightarrow 3.2 \times 10^{-8}$	$\rightarrow -17.25$
$55$	$\rightarrow 3.04 \times 10^{-3}$	$\rightarrow 2.63 \times 10^{-8}$	$\rightarrow -17.45$



slope  $\left\{ \begin{array}{l} R \\ \text{known} \end{array} \right. \Rightarrow$

$$E_a = 20.4 \frac{\text{kJ}}{\text{mol}}$$