

Transformation of Data

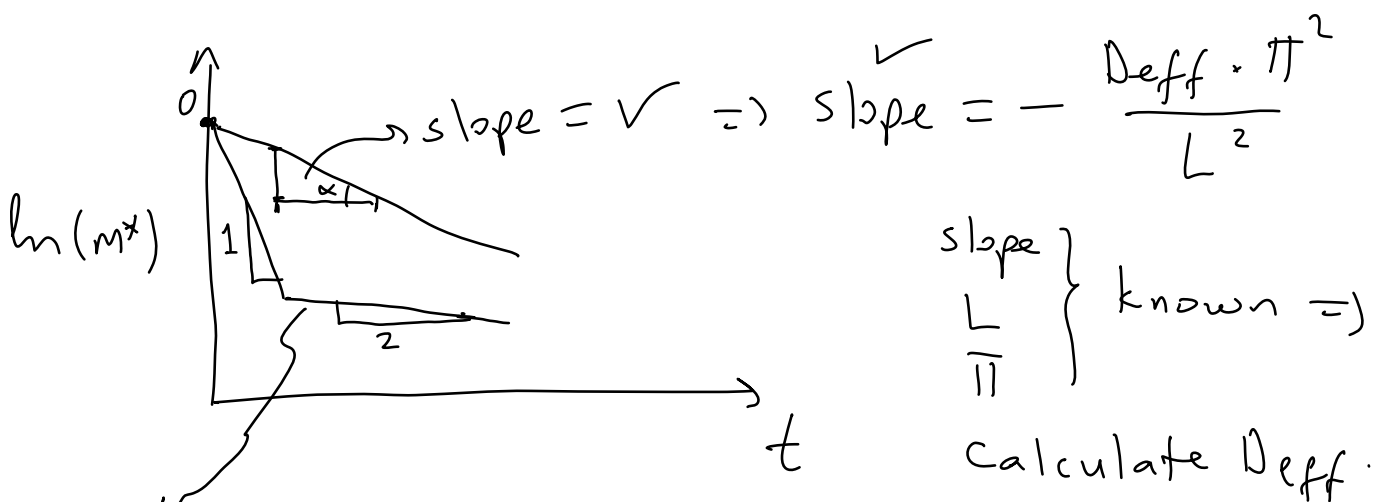
* D_{eff} is typically determined by plotting experimental drying data vs time.

X	t	m^*
\vdots	\vdots	\Rightarrow calculate
\vdots	\vdots	\vdots

For a sphere \Rightarrow

$$m^* = \frac{X - X^*}{X_0 - X^*} = \frac{6}{\pi^2} \cdot \exp\left(-\frac{D_{eff} \cdot \pi^2 \cdot t}{L^2}\right)$$

$$\ln(m^*) = \ln\left(\frac{6}{\pi^2}\right) - \frac{D_{eff} \cdot \pi^2 \cdot t}{L^2} \quad \leadsto \text{linear eqn}$$



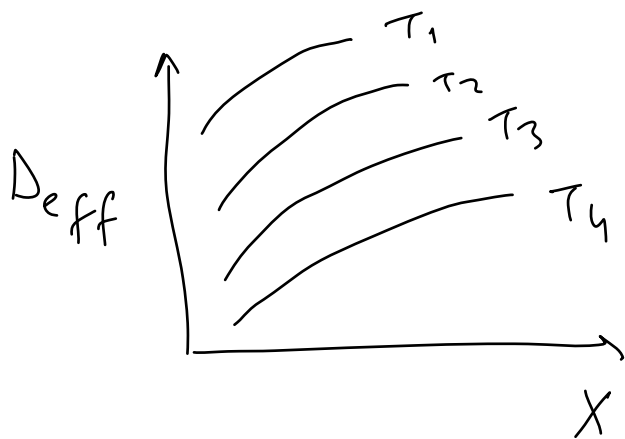
two falling rates $\Rightarrow D_{eff1}$ and D_{eff2} \leftarrow

$$D_{eff1} > D_{eff2}$$

* D_{eff} changes with MC and T.

as $T \uparrow \Rightarrow D_{eff} \uparrow$

as $MC \downarrow \Rightarrow D_{eff} \downarrow$



$$T_1 > T_2 > T_3 > T_4$$

* The temperature dependence of diffusivity is described by an Arrhenius type equation.

$$D_{eff} = D_0 \times \exp\left(-\frac{E_a}{RT}\right)$$

D_0 : diffusivity constant.

When $T \rightarrow \infty \Rightarrow D_{eff} \approx D_0$

E_a : activation energy (kJ/mol)

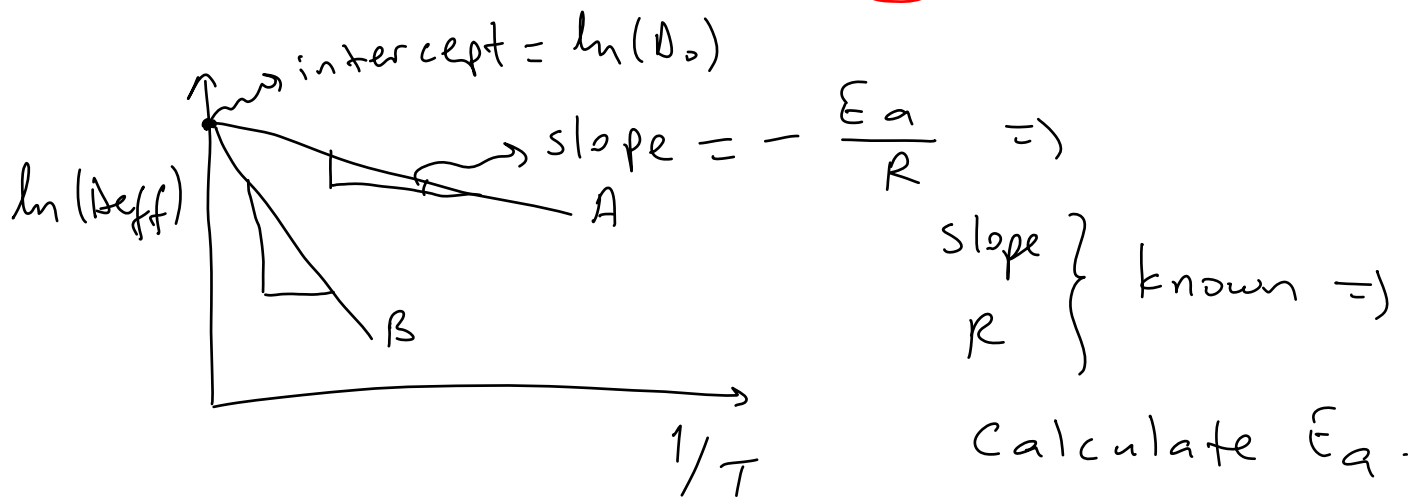
R : gas constant (8.314 kJ/mol.K)

T : absolute temp. (K).

⊗ E_a values are in the range of $15 - 40 \frac{\text{kJ}}{\text{mol}}$ for various foods.

⊗ The E_a can be determined by plotting $\ln(D_{\text{eff}})$ vs $1/T$.

$$\ln(D_{\text{eff}}) = \ln(D_0) - \frac{E_a}{R} \cdot \frac{1}{T}$$



The food B is more T sensitive than A.

i.e., D_{eff} values of B varies with T easily than A.

i.e., it is not necessary to dry A at very high T 's. Because D_{eff} value doesn't change with T . It is important to dry it at possible minimum temperatures in order to save energy and keep the quality properties of food at high levels.

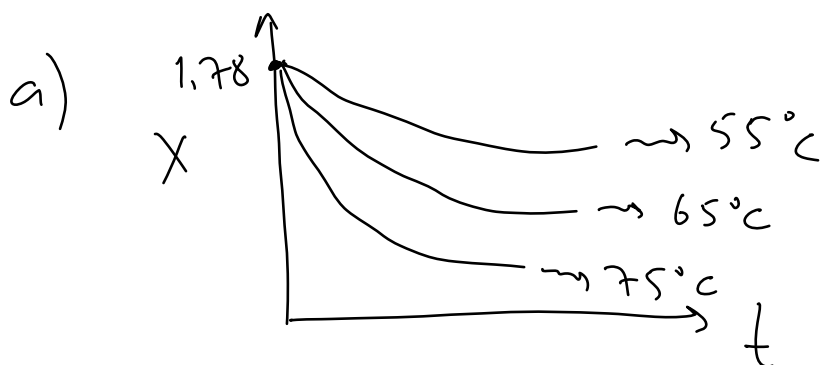
Example: 2.78 kg of grape leather (initial MC = 64 % wb) with a thickness of 1 mm was spreaded on a 0.06 m² area and dried in a tray dryer using hot air. Assume sample dries from the top surface only. A typical time (min)-MC (kg H₂O/kg dry solids) data were obtained as shown below:

- Plot MC vs time
- Plot drying rate (kg H₂O/m².min) vs MC
- Estimate diffusivity values
- Estimate E_a value.

Data:

<u>t (min)</u>	<u>X (75°C)</u>	<u>X (65°C)</u>	<u>X (55°C)</u>
0	1.78	1.78	1.78
10	0.85	1.19	1.31
20	0.36	0.71	1.00
30	0.21	0.39	0.61
40	0.13	0.22	0.39
50	0.11	0.14	0.23
60	0.098	0.11	0.18

Solution:

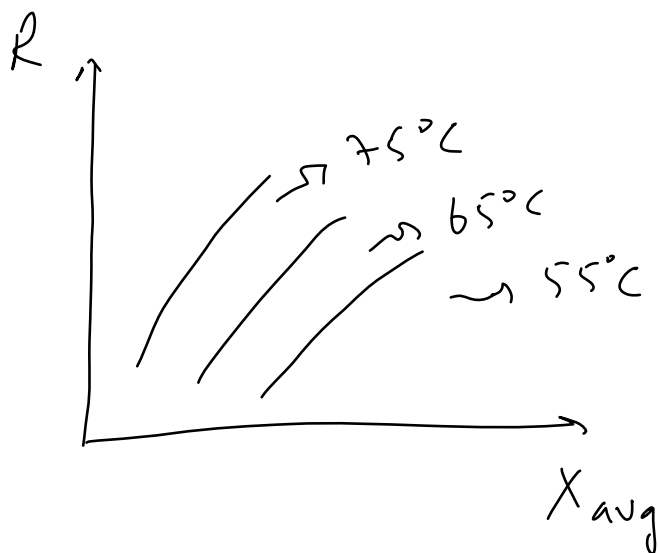


$$b) R = - \frac{M_s}{A} \times \frac{(X_{i+1} - X_i)}{(t_{i+1} - t_i)}$$

$$M_s = 2.78 \times (1 - 0.64) \cong 1.0 \text{ kg DS.}$$

$$\frac{M_s}{A} = \frac{1}{0.06} = 166.6 \text{ kg DS/m}^2 = \text{constant.}$$

$(t_{i+1} - t_i)$	$(X_{i+1} - X_i)$			X_{average}			R		
	<u>75°C</u>	<u>65°C</u>	<u>55°C</u>	<u>75</u>	<u>65</u>	<u>55</u>	<u>75</u>	<u>65</u>	<u>55</u>
10 →	-0.93	⋮	⋮ →	1.315	⋮	⋮ →	15.5	⋮	⋮
10 →	-0.49	⋮	⋮ →	0.605	⋮	⋮ →	8.16	⋮	⋮
10 →	-0.15		→	0.285		→	2.5		
10 →	-0.08		→	0.17		→	1.33		
10 →	-0.02		→	0.12		→	0.33		
10 →	-0.012		→	0.104		→	0.2		



} drying is in the falling rate period.

Calculate $t_f \Rightarrow$

$$t = \frac{M_s}{A} \left(\frac{x_1 - x_2}{R_1 - R_2} \right) \times \ln \frac{R_1}{R_2}$$

$$t_{75} = 166.6 \frac{\text{kg Ds}}{\text{m}^2} \cdot \frac{(1.78 - 0.098) \frac{\text{kg H}_2\text{O}}{\text{kg Ds}}}{(15.5 - 0.2) \frac{\text{kg H}_2\text{O}}{\text{m}^2 \cdot \text{min}}} \times \ln \left(\frac{15.5}{0.2} \right)$$

$$t_{75^\circ\text{C}} \approx 79.67 \text{ min.}$$

t_{65} and $t_{55} \Rightarrow$ calculate at home.

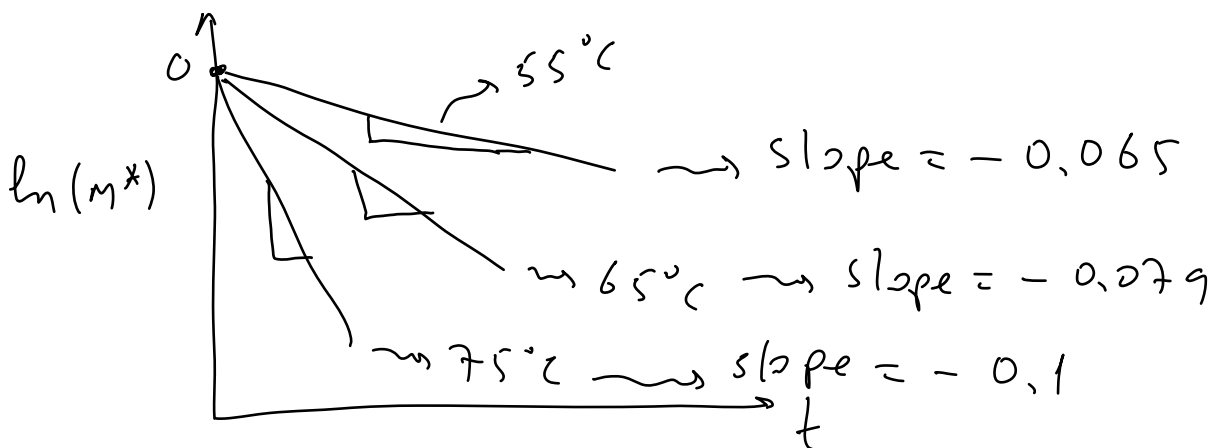
c) Assume slab shape \Rightarrow

$$m^* = \frac{x - x^*}{x_0 - x^*} = \frac{8}{\pi^2} \exp \left(- \frac{\pi^2 \cdot \text{Deff} \cdot t}{4 \cdot L^2} \right)$$

$$\ln(m^*) = \ln \left(\frac{8}{\pi^2} \right) - \frac{\pi^2 \cdot \text{Deff} \cdot t}{4 \cdot L^2}$$

T	x_0	x^*	For $75^\circ\text{C} \Rightarrow$	
75	$\rightarrow 1.78$	$\rightarrow 0.098$	t	m^*
65	$\rightarrow \dots$	$\rightarrow 0.11$	0	$\rightarrow 1$
55	$\rightarrow \dots$	$\rightarrow 0.18$	10	$\rightarrow 0.44$
			20	$\rightarrow 0.15$
			\vdots	\vdots
			60	\vdots

t	m^*			$\ln(m^*)$		
	75°C	65°C	55°C	75	65	55
0	1	1	1	0	0	0
10	0.44	⋮	⋮	-0.80	⋮	⋮
20	0.15	⋮	⋮	-1.85	⋮	⋮
30	0.06			-2.7		
40	0.01			-3.9		
50	0.007			-4.9		
60	0			∞		



$$\text{slope} = - \frac{D_{\text{eff}} \cdot \pi^2}{4 \times L^2}$$

$$\text{For } 55^\circ\text{C} \Rightarrow -0.065 = - \frac{D_{\text{eff}} \cdot \pi^2}{4 \times (1 \times 10^{-3})^2 \text{ m}^2} \Rightarrow$$

$$D_{\text{eff}} \text{ at } 55^\circ\text{C} = 2.63 \times 10^{-8} \text{ m}^2/\text{min}$$

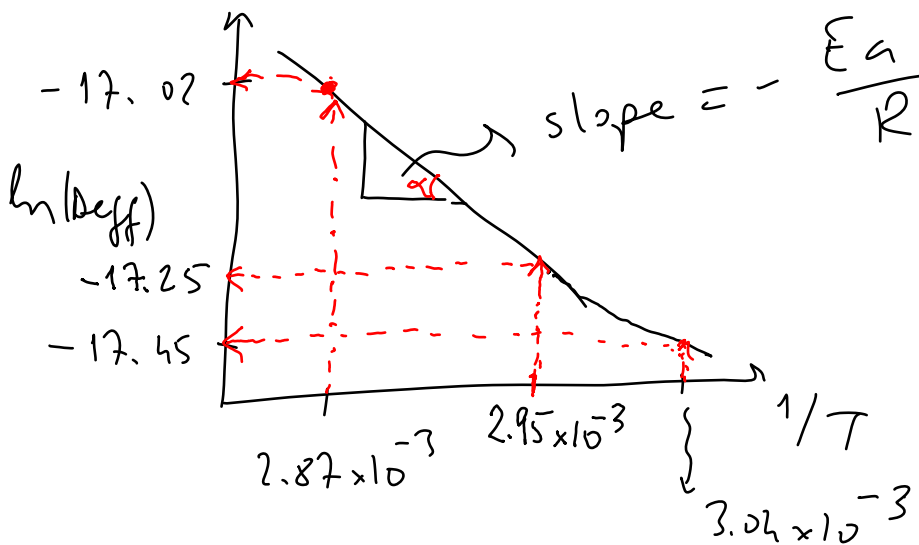
$$D_{\text{eff}} \text{ at } 65^\circ\text{C} = 3.2 \times 10^{-8} \text{ m}^2/\text{min}$$

$$D_{\text{eff}} \text{ at } 75^\circ\text{C} = 4.056 \times 10^{-8} \text{ m}^2/\text{min}$$

$$d) D_{eff} = D_0 \times \exp\left(-\frac{E_a}{RT}\right) \Rightarrow$$

$$\ln(D_{eff}) = \ln(D_0) - \frac{E_a}{RT}$$

T	$1/T$	D_{eff}	$\ln(D_{eff})$
75 + 273	$\rightarrow 2.87 \times 10^{-3}$	$\rightarrow 4.056 \times 10^{-8}$	$\rightarrow -17.02$
65 "	$\rightarrow 2.95 \times 10^{-3}$	$\rightarrow 3.2 \times 10^{-8}$	$\rightarrow -17.25$
55 "	$\rightarrow 3.04 \times 10^{-3}$	$\rightarrow 2.63 \times 10^{-8}$	$\rightarrow -17.45$



slope $\left\{ \begin{array}{l} R \\ \text{known } \Rightarrow \end{array} \right.$

$$E_a = 20.4 \frac{\text{kJ}}{\text{mol}}$$